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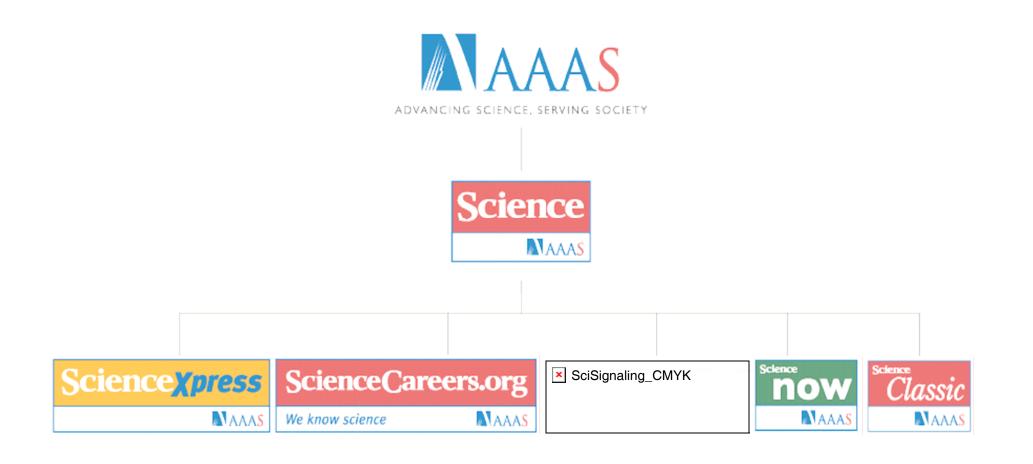


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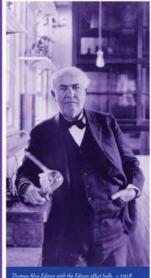
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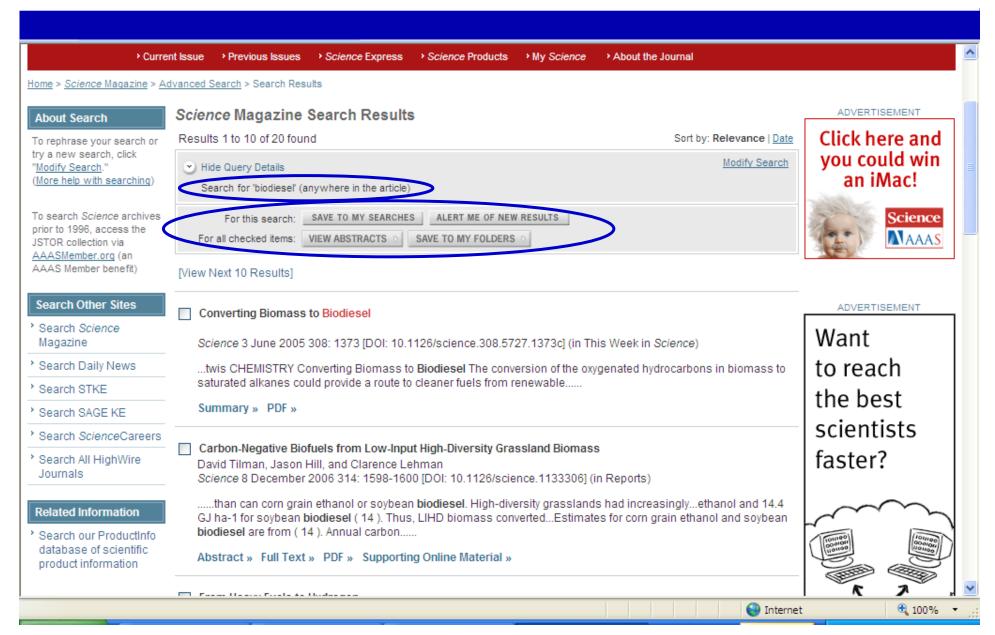












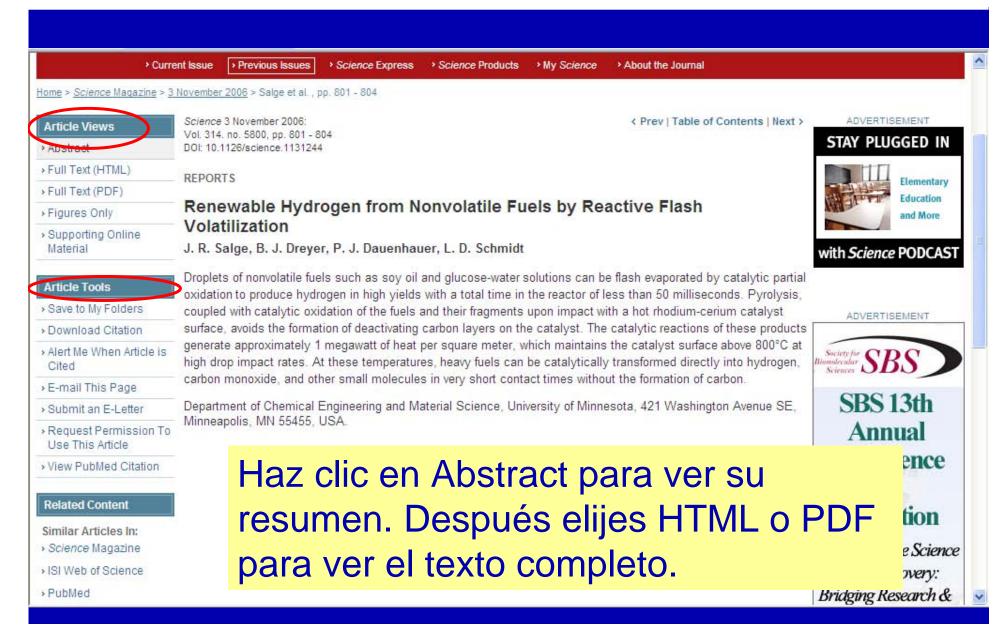


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spray ~400-µm-diameter drops onto a catalyst foam containing Rh-Ce catalyst particles at typically 2.5% by

directly on the front face of the catalyst. Air flowed around the fuel injector to provide a uniform flow field and to

antimize miving with the account products. Air and fuel enter at 20°C: no external heating was needed

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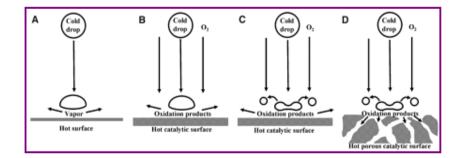


Fig. 3. Sketches of possible configurations of (A) conventional film boiling of a volatile drop on a hot surface, (B) reactive drop volatilization on a hot catalyst surface, (C) dropimpingement and breakup on a hot catalytic surface, and (D) drop impingement and breakup on a hot catalytic porous surface. [View Larger Version of this Image (71K JPEG file)]

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experiments, long-term evaluation, and modeling to optimize catalyst performance and determine the exact

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- 14. Our system processes approximately 0.6 kg/day of fuel diameter would process ~5.2 kg/day under identical co fuel injectors to obtain sufficiently low flows, but larger injectors, or different methods for uniform drop formation
- This research was supported by grants from the U.S. De Initiative for Renewable Energy and the Environment at

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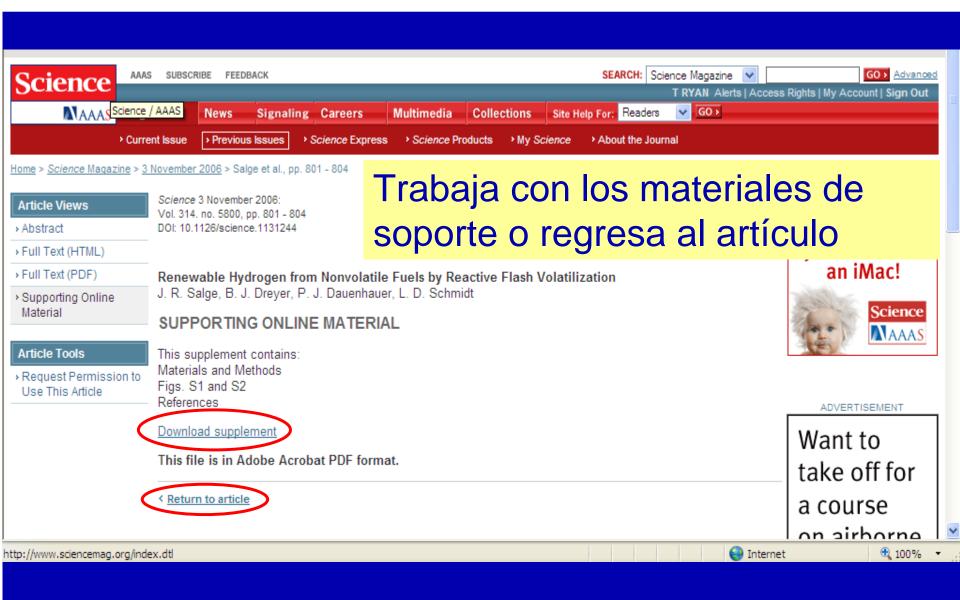
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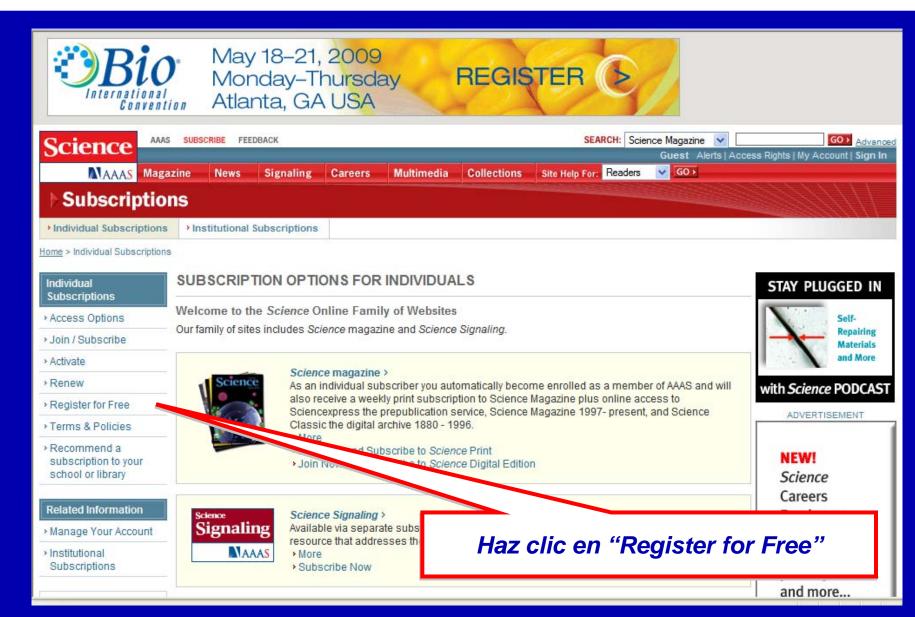
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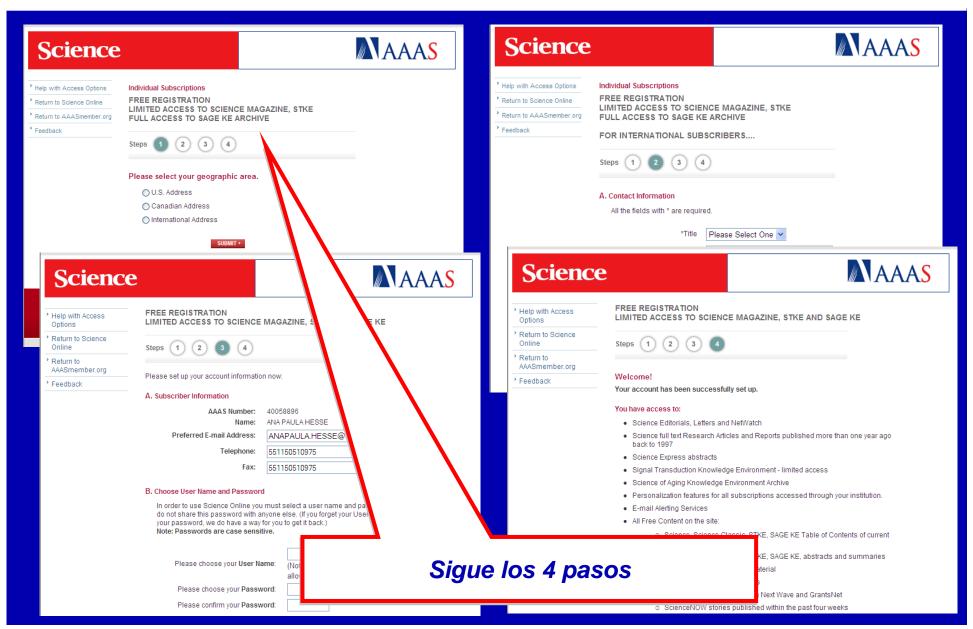






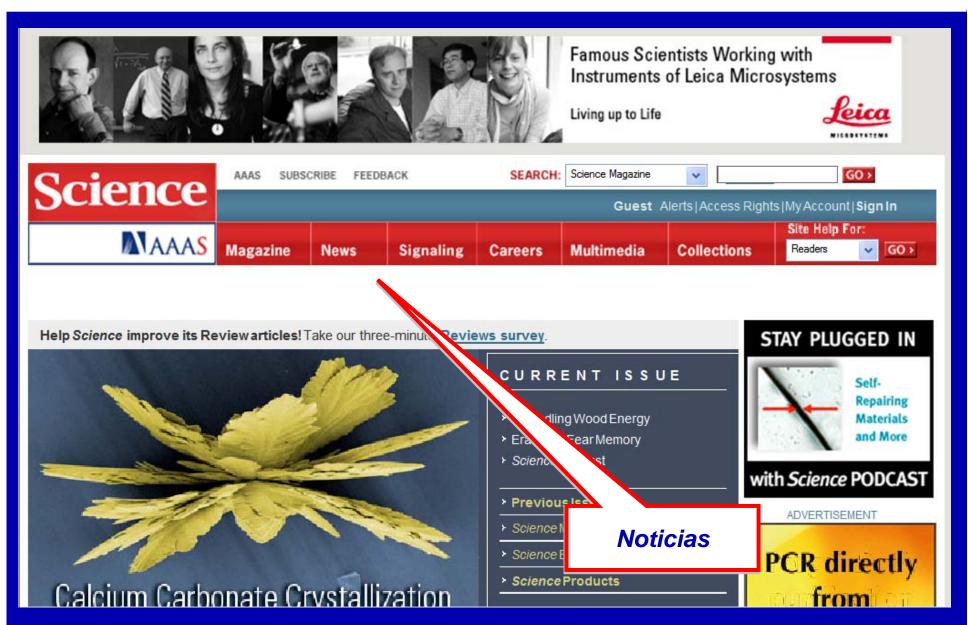






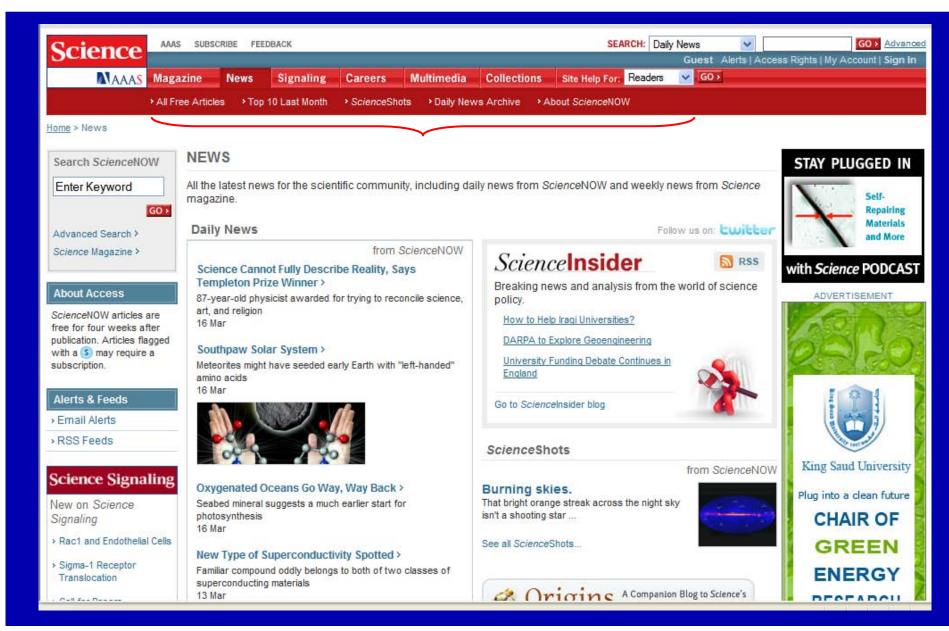
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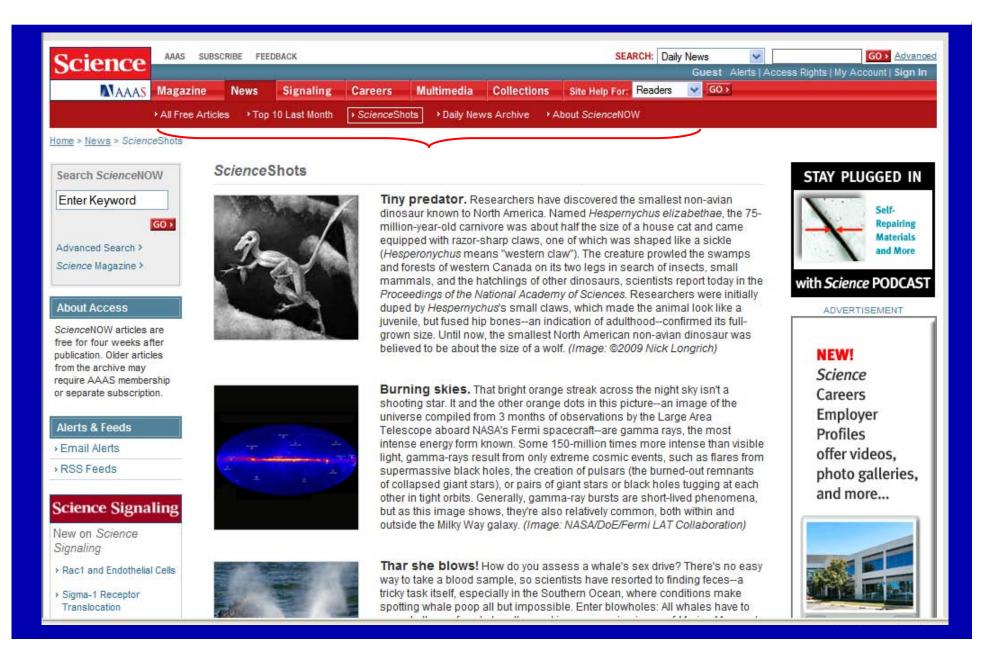
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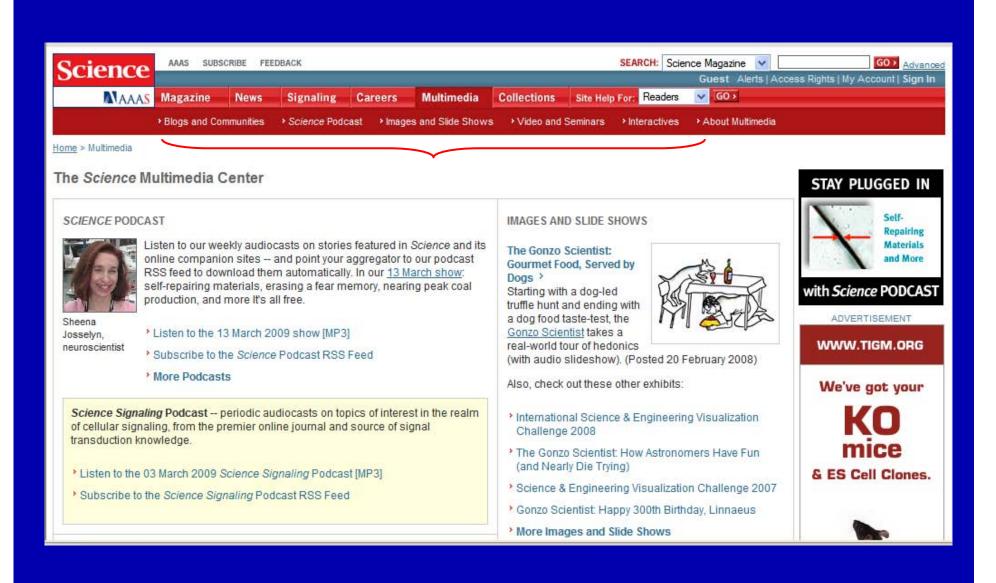
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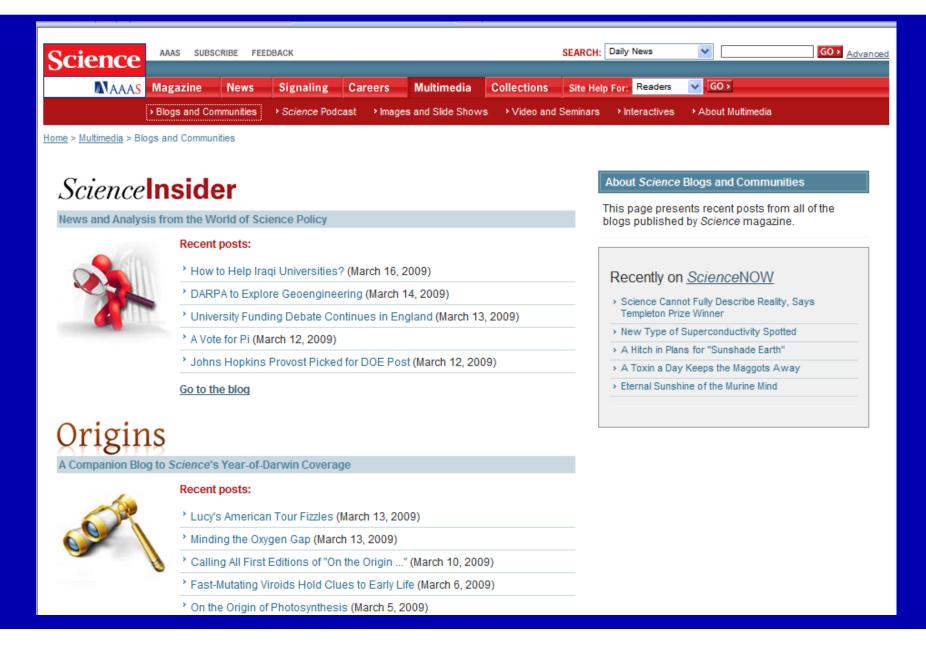
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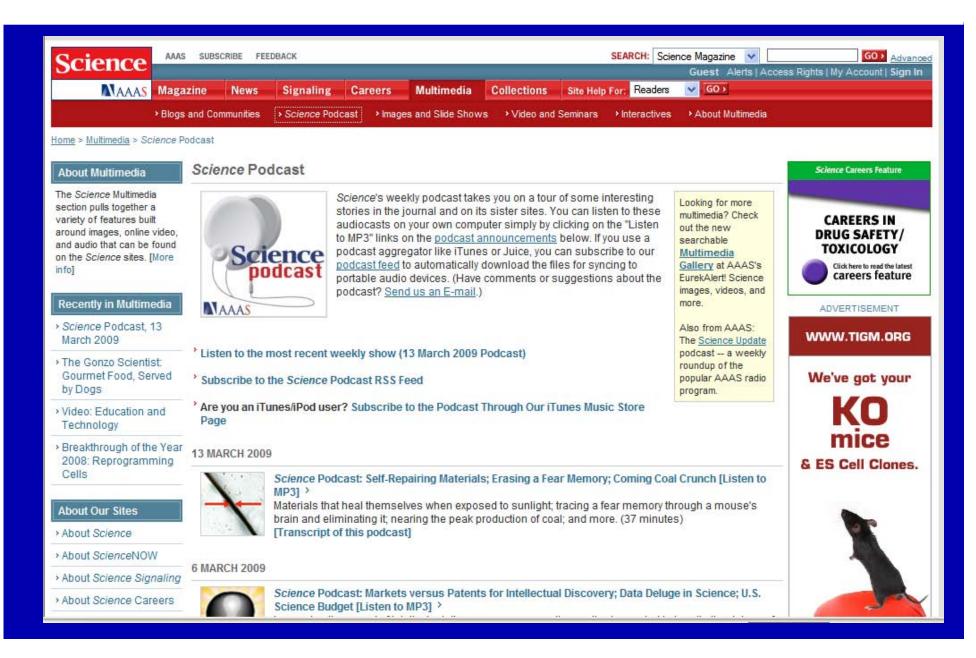
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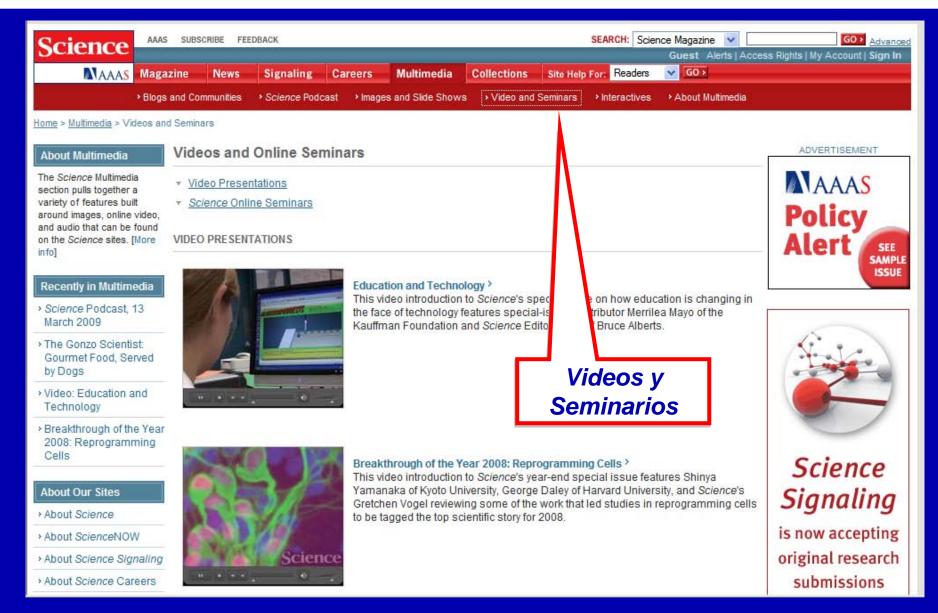
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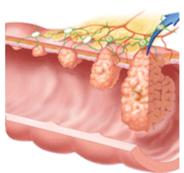
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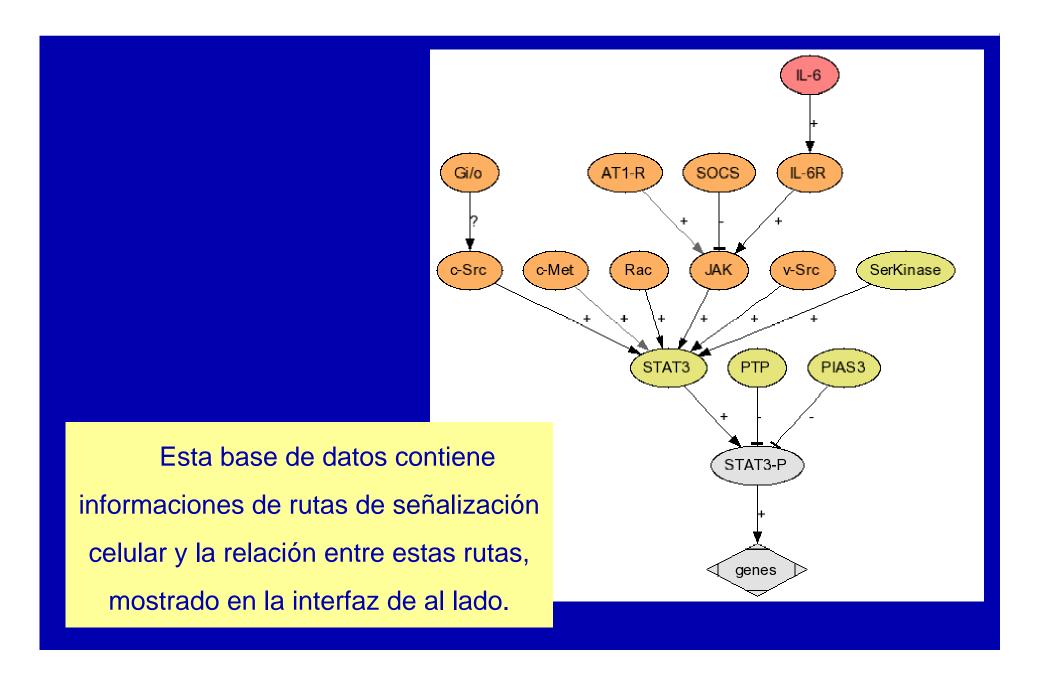
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